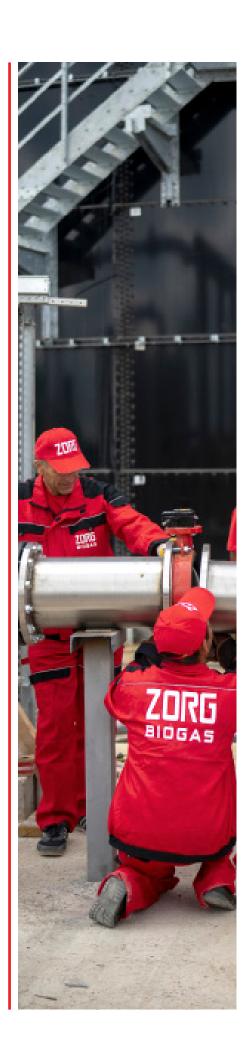


### Proposal

BioCNG plant 10 tpd using Napier grass



Date: 10/04/2024 Validity: 3 months



#### **CONTENT**

Overview	3
Raw material potential	4
Biogas plant characteristics	5
Working principle	6
Technological process of biogas production	7
Main equipment	8
Solid feeder	9
Reactor	10
Reactor vertical agitator	11
Window with spotlight	12
Pump equipment	13
Separator	14
Receiving tank and Filtrate tank	15
Submersible mixer	16
Gasholder	17
Biogas cooling system	18
Biogas compressor	19
Desulphurization system	20
Biogas burner	21
Water supplying and sewerage system	22
Heating system	23
Dry cooler (cooling substrate system)	24
Automation and electrical equipment	25
Sensors set	26
Laboratory	27
Specification list	28
Appendices:	33
Appendix 1. Material flow diagram	34
Appendix 2. Basic diagram	35
Appendix 3. Plan of biogas plant	36
Appendix 4. Electric power consumption	37
Appendix 5. Equipment price	38
Appendix 6. Price	39
Appendix 7. List of exclusions	41



#### **OVERVIEW**

We offer a solution to process Napier grass to biogas in high-load reactors (HLR). The proposed HLR technology is superior to the coventional CSTR. HLR is 3 times smaller and cheaper than CSTR. For 10 tonnes bioCNG a day just 1 HLR x 4150 m³ is enough.

Zorg makes the detailed engineering, supplies the equipment and provides supervision during construction as well as training and start-up. Zorg' part makes 49% from the total budget.

The construction and installation are done by Customer under Zorg' supervision and quality control. A purification from CO2 and compression 250 bar are an option. Customer may order this from Zorg or locally himself. The local part is 51%.

# Raw material potential

Biomethane (m³/day)	13 723
Methane content (%)	52
Biogas (m³ /day)	26 231
Biogas yield (m³ / tonneODM)	069
ODM quantity (tonnes / day	38.02
DM quantity (tonne s/ day)	39.6
ODM content (%)	96
DM content: (%)	33
Quantity (tonnes/year)	43 800
Quantity (tonnes/day)	120
Substrate	Napier grass

#### **Biogas plant characteristics**

Characteristics	Values	Figures
Number of reactors	units	1
Reactor		
a) volume:		
Work	$m^3$	3945
Overall	$m^3$	4152
b) Organic load	$kgODM/m^3$	9.64
c) Hydraulic retention time (gross)	days	35/33
d) Overall dimensions of the reactor		
(diameter / height)	m	23.0/10.0
e) Temperature	°C	+52
Gasholder		
a) Volume	$m^3$	870
b) Number of gasholders	units	1
c) Dimensions of the gasholder (diameter / height)	m	12.5/9.3

#### Number of personnel

	Shift 1	Shift 2	Shift 3
Operator	1	1	1
Electrician	1	-	-
Mechanic	1	-	-
Total	5		



#### Biogas plant working principle

The technology is based on the biochemical conversion of organic materials from high molecular weight compounds to low molecular weight compounds. The first stage of this process is hydrolysis. Hydrolysis produces organic acids and alcohols. Organic compounds + H2O→ C5H7NO2+H-CO3.

Further conversion of obtained dissolved compounds like organic acids and alcohols (C5H7N02,HC03) into gases - CH4, CO2. C5H7N02+HC03+H20 $\rightarrow$ CH4+C02+NH4.

Biological process of consecutive (phasic) conversion of organic compounds take place in anaerobic environment i.e. in oxygen-free tank (biological reactor). At the first stage of fermentation, substrate hydrolysis take place under acidogenic bacteria influence. At the second stage, elementary organic compounds come through hydrolysis oxidation by means of hetero-acidogenic bacteria with production of acetate, carbon dioxide, and free hydrogen. The other part of the organic

compound including acetate forms C1 compounds (elementary organic acids). Produced substances are the feedstock for methanogenic bacteria of the third type. This stage flows in two processes of A and B type the character which depends on caused by different bacteria type. These two types of bacteria convert the compound obtained during the first and second stages into methane CH4, water H20 and carbon dioxide CO2. Methanogenic bacteria are more sensitive to the living environment compared to acidogenic bacteria. They require a complete anaerobic environment and a longer reproduction period. The speed and scale of anaerobic fermentation depends on bacteria metabolic activity. That is why the biogas plant chemical process includes hydrolysis stage, oxidation, and methanization stage. For that kind of substrate, these processes take place in the same reactor

#### Technological process of biogas production

Napier grass is transported to a biogas plant area and discharged into loaders. loaders input substrates portion to reactors using In the reactors the substrate is brought up to a temperature of +52°C. Constant temperature is sustained for the entire digesting period. To prevent a rise in temperature (for example, in summer), the biogas station is equipped with a coolers (dry cooling). The reactors operating regime is thermophilic. The heated substrate in the digesters is blended periodically. Mixing is performed by vertical agitators. The average time of processing in the reactors is 32 days. After the reactors, the substrate is fed by pump to a separator area where it is separated into solid and liquid bio-fertilizer. Solid bio-fertilizer is discharged to the separation area and transported for storage; liquid filtrate is directed to a liquid residue storage tank. Biogas goes up under overlap and delivered into an external gas holder through pipeline.

The gas holder's weather protective film protects the gasholder from precipitation and damage by foreign objects. The weather protective film is fixed firmly by a special system. To protect the gasholder from overpressure, digesters are equipped with safety valves, which start working at a pressure of 5 mbars and bleeds biogas to the atmosphere.

Then accumulated in gasholders biogs goes through a gas pipeline to a biogas cooler with a condensate discharge unit and then to a compressor, where the pressure is raised up to 80-150 mbar to meet engine requirements. After the compressor, biogas is fed to activated coal filters to remove hydrogen sulfide (H2S). After filters, biogas goes to biogas upgrading plant where raw biogas treats through the removal of CO2 and other soluble gases to produce primarily methane gas (~99%) which is clean and dry.

All technological processes are controlled and operated by an automatic system. Biogas plant work is monitored at the central control room monitor. The control room is equipped with a central control unit, which allows the switching of any biogas plant module into automatic or manual mode with local or remote control.

#### MAIN EQUIPMENT





#### Solid feeder (SF-01)

Solid feeder machines have been proven in various situations. Solid feeder has the solid design, which guarantees a maximum functionality and less maintenance, combined to a low energy consumption. Because of the vertically oriented walls, there is no change for the material to get stuck or build bridges. The conveyor chains and the milling-unit allow continuous dosing by various types of materials. Furthermore, the material is loosened by this dosing process. The user is able to control the material flow up to  $20 \, \mathrm{m}^3 / \mathrm{h}$  or more, regarding to the own consumption of electrical power by the machine. In addition, the corrosion protection, wear resistance and high quality allow customers to use our product for a long period of time.

#### **Specifications**

Length:	13.7 m
Width:	2.5 m
Height	3.4 m
Volume:	50 m <sup>3</sup>
Quantity:	1 pcs.



#### Reactor (RT-01)

Reactor is a tank of cylindrical form (for better mixing during the fermentation). It is built of cast-in-situ reinforced concrete based on sulphate-resistant cement with thickness of walls and bottom - 0,25m. In the center of the reactor there is a column with chapiter. Overlap of reactor is reinforce concrete plate. On the tank's wall and in the bottom there is to be installed pipelines for heating, intended for assurance and maintenance of the optimal fermentation process temperature at thermophilic conditions. For heat conservation and reduction of heat energy con-

sumption, the reactor walls, overlap and bottom are insulated outside with 100 mm slabs of extruded polystyrene foam. Over the heater, the substructure walls and bottom are insulated with roll damp proofing. Superstructure and substructure heat insulation is protected by shaped sheet from the outside mechanical damages and rodents. The reactor`s bottom has a slope 1%.

#### **Specifications**

Height:	10,0 m
Diameter :	23,0 m
The total volume : The substrate volume :	4152 m³ 3945 m³
Quantity:	1 pcs



#### Reactor vertical agitator (AG-01 ... AG-05)

Vertical agitators are designed and engineered to guarantee high energy efficiency. We use gear units and motors from respected European manufacturers. This guarantees the long life of our mixers. All motors and gear units are available with ATEX certifications. Agitators are designed for mixing substrates with a high solids content of 13-18%. The blades of the mixers are set at an optimum angle, and the external motor of the mixer is mounted on a special support.

#### **Specifications**

**Engine power:**Quantity per digester:
Quantity total:
5 pcs
5 pcs



#### Window with spotlight (SG-01)

Inspection windows are designed for visual control of processes inside the fermenter. Spotlights were made in explosion-proof with automatic disconnection. Inspection windows are equipped with a cleaning washing system.

#### **Specifications**

Inspection windows Ø300 Spotlight VISULUX UL50 -G -H 230V, 50W, IP65



#### Pump equipment (PU-01, PU-02, PU-03)

Pumps are used to transport substrate to the equipment and facilities in the biogas plant and away. Biogas plant design allows to access easily to all pumps. Pumps are driven by helical geared motor. Stator has hopper inlet for optimum filling of the pumping chamber, wear-protected, robust universal joint with feeding screw, robust bearing pedestal with close-coupled drive and self-centering of the drive shaft. Pumps have modular design for high flexibility, low life-cycle-costs.

#### **Specifications**

Flow rate: 30 m3/hour **Engine power:** 7.5 kW Pressure: 4 bar Quantity: 2 pcs

Liquid substrate pump (PU-02) 30 m3/hour Flow rate: 7,5 kW **Engine power:** 4 bar Pressure: 1 pcs Quantity:

Filtrate pump (PU-03)

30 m3/hour Flow rate: 7,5 kW **Engine power:** 4 bar Pressure: 1 pcs Quantity:



#### Separator (SR-01)

The Press Screw Separator covers a broad spectrum of applications, from agriculture to biogas and bioethanol plants. The innovative technology separates substrates in its solid and liquid elements. The secret of the versatility of the press screw separator is that it can adjust to different dry matter contents and Thick liquids (20% dry matter content). Slotted screens have different assortment and width of table cells and give possibility work with small solids and fiber contents. In the slotted screen, the solids are screened out from the liquid. The solids build up a layer which also acts as a filter to separate finer particles from the liquid. The auger flights convey this layer to the solids outlet. The screen surface is cleaned and a new filter layer is formed. The design of the screens is not conducive to plugging. The pressure in the first part of the screen is low but increases with the solid consistency to the solid output. The consistence of the gained solid can be varied with the help of a output regulator by the amount and position of counter weights. This way the required consistency of the final product for either further storage, use as fertilizer or the basis for compost can be reached. The liquid phase can easily be drained through a pipe or hose system.

#### **Specifications**

Engine power 5,5 kW

Flow rate 5-10 m<sup>3</sup> / h

Quantity 1 pcs

Equipment Frame

Screw Sieve for the filtration

Counterweights

The design of the protective room



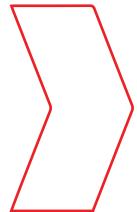
#### Receiving tank (RT-01) and Filtrate tank (FT-01)

Reinforced concrete tank for the storage of liquid raw materials. The tanks are equipped with level sensors and submersible agitators for mixing the substrate.

#### **Specifications**

Receiving tank (RT-01) Diameter: Height Total volume:	6.0 m 2.5 m 75 m³
Quantity:	1 pcs
Filtrate tank (FT-01) Diameter: Height Total volume:	6.0 m 2.5 m 75 m³
Quantity:	1 pcs





#### Submersible mixer (AG-06, AG-07)

The submersible motor agitator serves for mixing renewable raw materials (RRM), liquid substrate as manure and similar substrates. The electro-motor driven submersible agitator is designed for submersion operations in potentially explosive environments of Ex zone 2 and complies with Directive 94/9 EC. The submersible agitator can be attached to most sliding masts by means of the motor support. A mounting option for a hauling cable is provided on the motor support for height adjustment purposes.

Due to the 4-roller guidance of the motor support, the agitator can be lifted and lowered without friction and the square mast, even if the pull of the hauling cable is slightly angular. The motor support is designed for a  $100 \times 100$  mm square sliding mast as standard, but can also be used for an  $80 \times 80$  mm sliding mast by changing the

rollers. The strain relief of the connecting cable can be positioned in the extension of the motor or towards the top on the motor support, depending on the requirements. This enables universal utilization with the most various installation kits.

The geared motor is made of spheroidal graphite iron(GGG40) and painted, the propeller is galvanized and the motor support is made of stainless steel. The submersible motor agitator is designed as a water pressure-tight monoblock unit for driving the three-vane propeller. The submersible agitator is of modular design, submersible electro-motor with flange-mounted planetary gear and bearing flange for holding the propeller. The conical shaft in the bearing flange is mounted in the oil bath by two angular roller bearings and sealed off from the agitating substrate with a mechanical seal.

#### **Specifications**

Submersible mixer of the receiving tank (AG-06)
Nominal power
Quantity:

N=5.0 kW 1 pcs

Submersible mixer of the filtrate tank (AG-07)
Nominal power
Quantity:

N=3.0 kW 1 pcs



#### Gasholder (GH-01)

The gasholder provides for biogas stor- The biogas pressure in the gasholder is 2-5 age and for equalizing pressure and bio- mbar. The membranes are designed and gas composition. The gasholder system cut out on NC machines. Welding is exehas a two-layer construction. The external cuted by high frequency currents. These material consists of a weather-proof film steps yield substantial improvements for of PVC-coated polyester fabrics with UV quality and service life compared to handprotection. Both sides are finished with an made membranes welded by standard external N/5cm, internal membrane PELD welding equipment. (gasholder) membrane.

ture range allows operation from -30°C to stalled on the external membrane.

The internal film is stretched under normal biogas pressure. Air is blown into the space between the external and internal membranes to pressurize the internal membrane and form the shape of the external membrane.

To prevent damage to the gasholder as a The gasholder has a methane permeation result of overpressure conditions, a safemaximum of 260 cm3/m2 \* 1 bar biogas ty valve is installed. To survey the internal resistance. The gasholder film tempera- membrane, an inspection window is in-

#### **Specifications**

9.3 m Height: Diameter: 12.5 m The total/working volume: 870 m<sup>3</sup> Quantity: 1 pcs



#### Biogas dryer and cooling (CHL-01)

Biogas dryer and cooling are provided with special equipment as GAS COOLER and AIR-COOLED LIQUID CHILLER. Biogas plants thanks to an extensive range of dedicated Biogas solutions, low pressure heat exchangers, a comprehensive range of water chillers and RWD Dry Coolers. Designed as one-way shell-and-tube heat exchanger. Process gas inside of the tubes; cooling water in the shell. All parts in contact with the process gas made of stainless steel 316Ti or 316L; heat exchanger shell made of stainless steel/ Designed with gas outlet chamber outlet connection radial; inspection opening axial Official acceptance according to PED 2014/68/EU in accordance with ADMerkblätter and factory pressure test.

#### **Specifications**

Gas volume flow	990 m³/ h
Gas inlet temperature	+50 C
Gas outlet temperature	+10 C
Cooling power	150 kW
Engine power	42 kW



#### Biogas compressor (BC-01, BC-02)

Biogas blower is a device used to move gas and increase pressure thanks to a rotating impeller within a toroidal channel, so there is a progressive increase of energy.

Blower is used to transporting biogas from gasholder storage to consumer (biogas upgrading plant in our case).

#### **Specifications**

Flow rate:	990 m³/h
Pressure:	150 mba
Engine power:	16 kW
Quantity:	2 pcs



#### **Desulphurization system**

The desulphurization system is a 3-step system. Stage 1 is adding Ferrum Hydrooxide. Stage 2 - biological. Adding a certain portion of air to the fermenter. Air by special bacteria, converting H2S into S. After 1 and 2 steps the sulphur contcentration is 80 ppm. Stage 3 - activated charcoal filtration, as activated charcoal has the capability to absorb sulfur. After passing through activated charcoal filters, the sulfur concentration is re-duced to 0 ppm.

#### **Specifications**

Charcoal filter (CF-01)

The volume of charcoal: 300 kg

Numbers of charcoal columns: 1 pcs.



#### Flare (BF-01)

Flare is designed for the temporary or periodical complete combustion of the biogas produced by biogas plants without the possibility of its use as an energy source. The burn system consists of a burner and additional equipment. The burner is designed on the principle of injection and consists of a combustion nozzle with an injector with an air supply control system, flame protection tube, fitting and burner control system. The biogas combustion system is made of stainless steel.

The supporting structure holds the burner and vertically mounted socket. The burn control system is installed in a case, which is mounted on the supporting structure of the combustion system and contains all the elements for monitoring and controlling ignition and flame.

#### **Specifications**

Flow rate 990 m³/h Quantity: 1 pcs

#### Water supplying and sewerage system

Water supplying system provides biogas plant feed water, water for network circuits, the domestic water and fire safety systems. As used centrifugal single stage pumps as main pumping elements. These pumps are designed for pumping waste water, household / domestic water and sewage. Pressure Boosting Systems are designed for pure water pressure boosting in industrial plants. The booster comprises 2 to 3 (connected in parallel pumps) installed on a common base frame, and provided with all the necessary fittings.

#### **Specifications**

Drain pump Pressure 4m Flow 2-3 m3 / h Engine 0,24 kW

Equipment
Pump case control
Stove-base
gauges
Check valves
Float switches
Brackets
Valves

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22



#### **Heating system**

Heating equipment is using for biogas plant heating and for sustaining constant temperature in the fermenter. Heating equipment includes circulation pumps, heat exchanger, heating manifold and pipes. The heat from the boiler is transferred to the biogas plant by using heat exchanger, and then is pumped through of biogas plant by circulation pumps. A heat carrier prepares water with an additive of ethylene glycol. Inlet temperature in the fermenter is 60C, the outlet is 40C.

#### **Specifications**

Circulating pump feeding heat carrier

heating

Flow 30 m3 / h; Pressure 1 bar

Circulating pump feeding heat carrier to

the digester

Flow 18 m3 / h; Pressure 1.1 bar

The pumping station feeding propylene

glycol

Flow 0.8 m3 / h; Pressure 4 bar

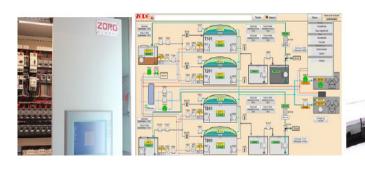


#### Dry cooler (cooling substrate system)

Device is designed to cool the substrate to working temperature according to technological regime. When use high temperature substrate, there is a chance of uncontrolled heating. The cooler is connected to the heating pipes, heat exchangers and it will be activated if it is need.

#### **Specifications**

Power (cooling)	100 kW
Length:	3,0 m
Width:	2,5 m
Height:	1,5 m
Power electrical	4 kW
Quantity:	1 pcs



#### **Automation and electrical equipment**

Process control equipment is used for supervision and regulation operation of the plant and for the limitation of damage. In case of emergency (for example, breakdown of the electrical power supply) the biogas plant is automatically transferred to safe operating conditions by the process instrumentation. Critical electrically driven devices are supplied with emergency power. An automatic system allows the supervision of the plant in real time and to recognize and correct aberrations immediately; to run the plant at its optimum saving resources and costs; and to record for the electronic database operation parameters. The automatic system consists of a control cabinet and sensors for parameter control of technological processes and execution devices.

The control cabinet is designed based on the industrial controller Siemens CPU315-DP2, using periphery distributing system Simatic ET200S, and operator panel OP277 Touch with touch-sensitive controls. Communications is executed by PROFIBUS and MPI with physical interface RS-485. The control program is designed based on the Simatic Step7. The control cabinet is a modular design. The upper part has a power box with central and front-end processor. The periphery distributing system, Simatic ET2005, is installed with input - output units. The lower part with interface relay and clips is installed for connecting execution devices. The entire plant is controlled by a single operator.

#### **Specifications**

Incoming control case with automatic set ASE-1, 2, 3
Base Siemens CPU315-DP2 controller
Peripherals Simatic ET200S
Control panel OP277 touchscreen
Communication PROFIBUS and MPI
Interface RS-485
Control system Simatic Step7

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25



#### **Sensors set**

Sensors are used to measure physical quantities (temperature, pressure, level of moisture) data collection.
installation kits

Conductometric sensor
Pressure Sensor / level
Ultrasonic sensor
Gas Pressure Sensor
Temperature converters with protective sleeves
The moisture sensor and the gas temperature



#### Laboratory

Monitoring and control of parameters of raw materials and fermentation processes is important for the efficient operation of a biogas plant. The laboratory allows you to assess the content of dry matter in the input raw materials, fermented mass, determine the ratio of volatile organic acids to total inorganic carbon (FOS/TAC parameter), determine the degree of substrate fermentation in fermenters, the level of biogas output, and evaluate the efficiency of separator.

#### **Equipment**

Analytical scales Moisture analyzer Automatic titrator Laboratory pH meter Centrifuge A set of flasks

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27

#### EQUIPMENT SPECIFICATION LIST



Nº	Equipment	Characteristic	Quantity
1	Loader	V=50 m³	1
1.1	Container bunker		1
1.2	Feeding screws	set.	1
2	Submersible mixer	N=3.0kW	1
2.1	Airtight motor gearbox		1
2.2	Hydraulic screw (wear-resistant steel)		1
2.3	Mixer control mechanism		1
2.4	Electric motor mount		1
2.5	Set of fasteners		1
3	Reactor vertical agitator	N=15 kW	5
3.1	Airtight motor gearbox		5
3.2	Hydraulic screw (wear-resistant steel)		5
3.3	Shaft (adapted to the height of the fermenter)		5
3.4	Blade		5
3.5	Frequency converter		5
3.6	Mounting bracket to bottom of the mixer		5
4	Safety valve of reactor		1
5	Window with a searchlight	set	1
5.1	Inspection window RD300 (mounts and sealant included)	Ø300	2
5.2	Spotlight (mount system bundled) VISULUX UL50 -G -H	230V, 50W, IP65	1
6	Substrate digested pump	30 m3/hour N=7.5 kW	1

Nº	Equipment	Characteristic	Quantity
7	Separator	N=5.5kW, Q=5-10m³/h	1
7.1	Body		1
7.2	Substrate Supply Pipe 4 ''		1
7.3	Engine - Gearbox	N=5,5 kW	1
7.4	Frame		1
7.5	Screw		1
7.6	Sieve for filtration		1
8	Filtrate pump	30 m3/hour N=7,5 kW	1
9	Liquid substrate pump	30 m3/hour N=7,5 kW	1
10	Submersible mixer	N=5.0 kW	1
11	PVC gas holder	860m³	1
11.1	Weather protection film	Ø12.5m	1
11.2	Gasholder film PELD methane permeation max.260 cm3/m2*d*1 bar, 650 N/5cm biogas resistant		1
11.3	Air blower	16A, 0,5kW	1
11.4	Excess and minimum pressure valve	0,0111	1
11.5	Dome level sensor		1
11.6	Mounting system		1
11.7	Accessories		1
11.8	Safety valve		1
12	Biogas Cooling System	990 m³/h	1
12.1	Chiller		1
12.2	Heat exchanger		1
12.3	Polypropylene glycol tank		1
13	Desulphurization system		1

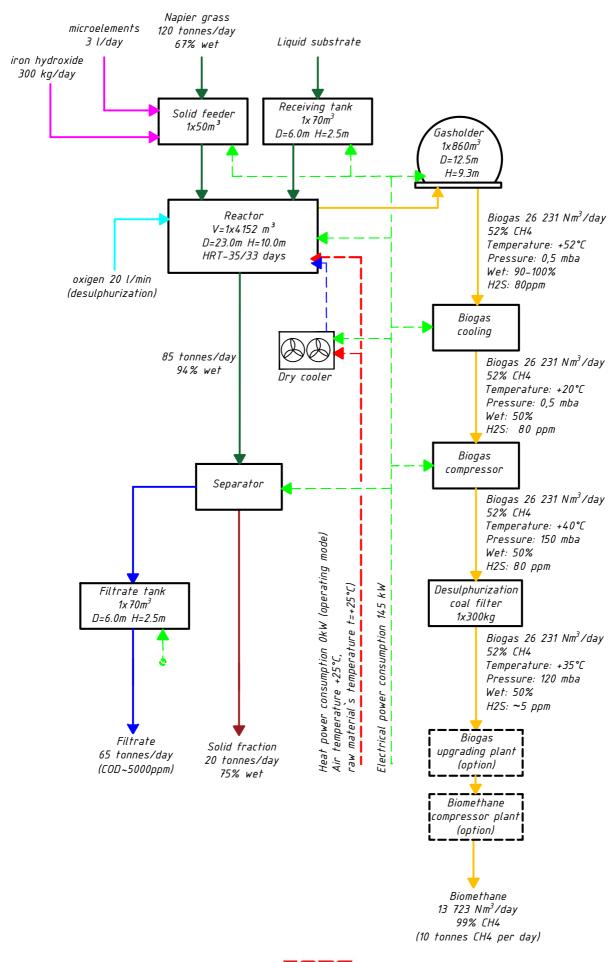
Nº	Equipment	Characteristic	Quantity
14	Biogas compressor	Q=990m³/h H=150mBar N=16kW	2
15	Electromagnetic flow meter		1
16	Flare	990 m3/h	1
17	Gas equipment included	set	1
17.1	Drainage pump with float	DN=50 Q=1m³/h H=13 m	2
18	The heat supply system	set	1
18.1	Diaphragm expansion tank	V=1000 l P=6Bar T=120°C	1
18.2	Circulating pump for supplying heat carrier	Q=30 m³/h H=1bar	
18.3	Propylene glycol feed pump station heating systems	Q=1,0 m³/h, H=4 bar	1
18.4	Circulation pump for supplying heat carrier to the digester	Q=18 m3/h, H=1.1 bar	1
19	Water supply and sewerage system, complete, disassembled	set	1
20	Automation with electrical equipment complete, disassembled	set	1
20.1	Incoming distribution cabinet with a set of automation DB-1		1
20.2	Incoming distribution cabinet with a set of automation DB-2		1
21	Sensors, set		1
21.1	Gas pressure sensor 0,025Bar		2
21.2	Gas pressure sensor 0,4Bar		2
21.3	Pressure sensor(substrate level) 1,0Bar		2
21.4	Pressure sensor (substrate pressure) 2,5bar		2

Nº	Equipment	Characteristic	Quantity
21.5	Resistive thermometer (gas temperature)		2
21.6	Resistive thermometer with thermo well (fermenter substrate temperature)		2
21.7	Resistive thermometer with thermo-well (digester tank substrate temperature)		2
21.7	Resistive thermometer (heat conductor temperature)		2
21.9	Conductometric sensor of maximum level		2
21.10	Conductometric sensor of water level		2
21.11	Dome position sensor		1
21.12	Coolant pressure sensor	SEN 3276 B065 G1/2 6Bar	2
21.13	Humidity and gas temperature sensor	ESFTF-I	2
22	Dry cooler 100kW heat pow.		1
23	Laboratory		1

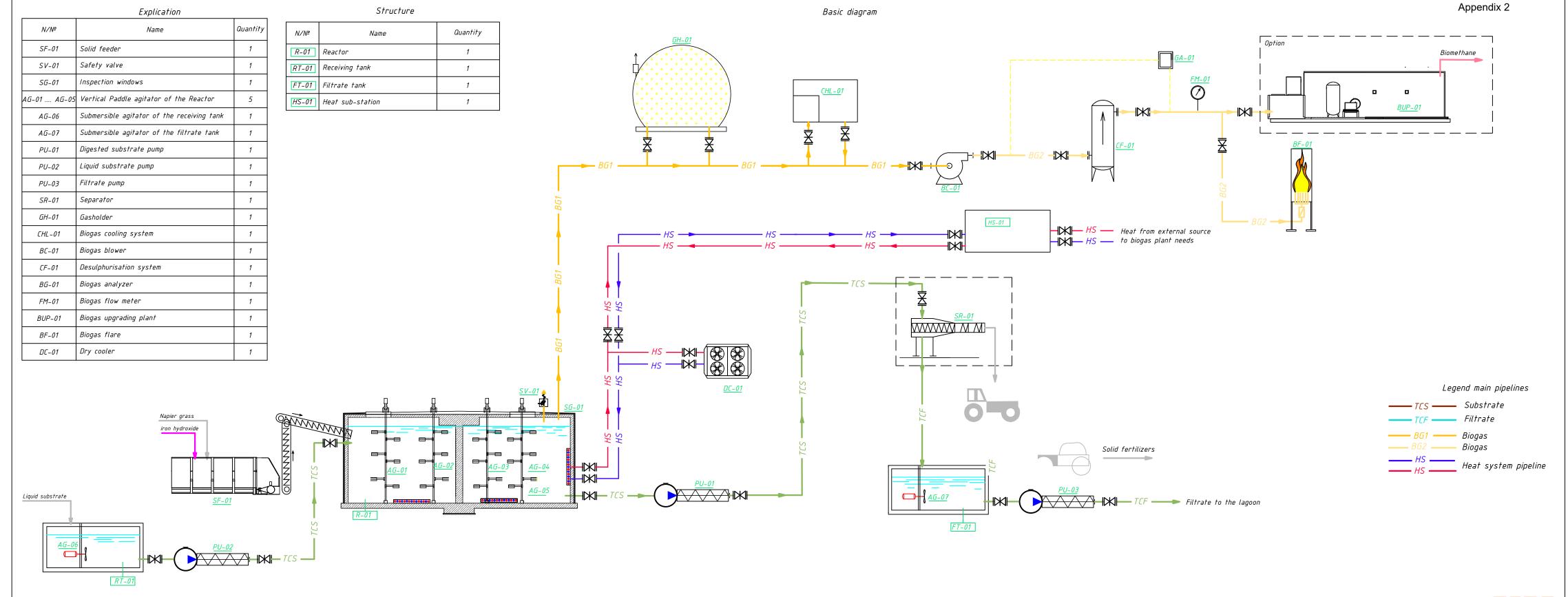
#### **APPENDICES**



#### **Material flow diagram**

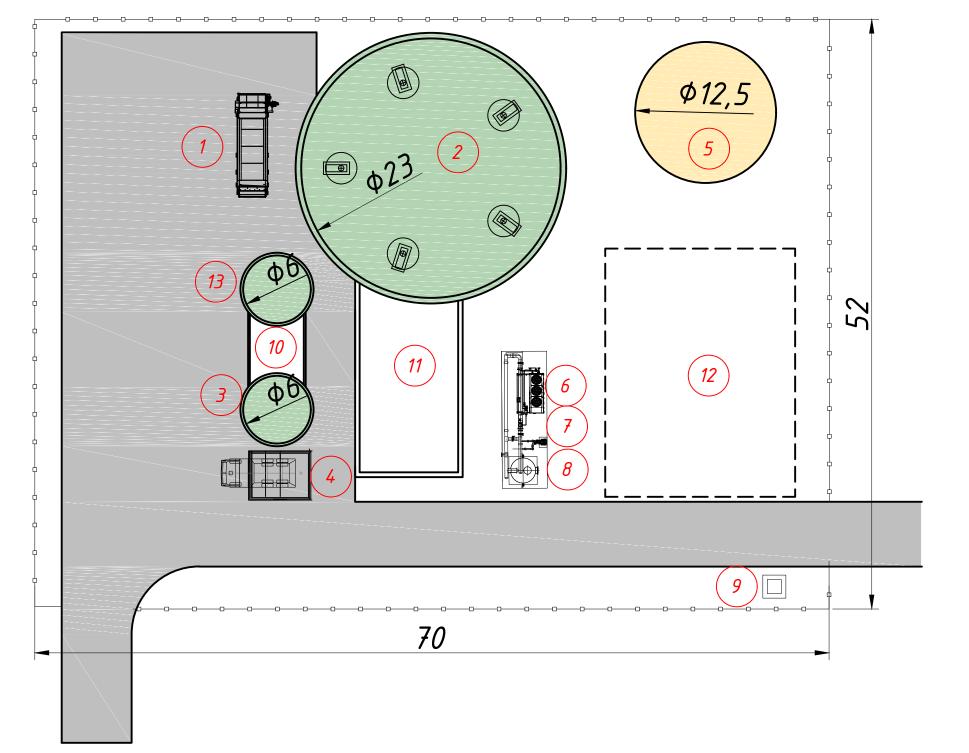








#### Plan



#### Explication

N/Nº	Name	Note
1	Solid feeder	SF-01
2	Reactor	R-01
3	Filtrat tank	FT-01
4	Separator platform	SR-01
5	Gasholder	GH-01
6	Biogas cooling system	CHL-01
7	Biogas compressor	BC-01
8	Carbon filter (desulphurization)	CF-01
9	Biogas burner	BF-01
10	Equipment room	ER-01
11	Technical room	TR-01
12	Biogas upgrading plant	BUP-01
13	Receiving tank	RT-01

Biogas plant area – 0,26 ha

Total plant area with options - 0,36 ha



#### Appendix 4

Electric energy consumption for own needs of the biogas plant					
Name equipment	Instal. Pow. (kW)	Q-y (pcs)	Total installed power (kW)	Working hours per day	Consumption kWh per day
Loader V=50 m <sup>3</sup>	22,0	1	22,0	8,0	176,0
Screw set.	16,5	1	16,5	8,0	132,0
Reactor Vertical agitator	15,0	5	75,0	18,0	1350,0
Submersible mixer in receiving tank	5,0	1	5,0	12,0	60,0
Submersible mixer in filtrate tank	3,0	1	3,0	12,0	36,0
Biogas cooling system	42,0	1	42,0	24,0	1008,0
Biogas compressor	16,0	2	32,0	12,0	384,0
Separator	5,5	1	8,0	8,0	64,0
Substrate pump to separator	7,5	1	8,0	8,0	64,0
Filtrate pump	7,5	1	2,0	4,0	8,0
Liquid substrate pump	7,5	1	2,0	4,0	8,0
Air compressor for gasholder lock	1,5	1	1,5	1,0	1,5
Air blower for double membrane	1,0	1	1,0	24,0	24,0
Digester cooling system	4,0	1	4,0	24,0	96,0
Circulation pump for supplying heat carrier to the digester	0,8	1	0,8	24,0	18,0
Circulation pump for supplying heat carrier to the digester cooling system	2,0	1	2,0	24,0	48,0
Circulating pump feeding hot water at technical building	0,1	1	0,1	24,0	1,9
Propylene glycol pump station	0,8	1	0,8	0,5	0,4
Drinage pump	1,0	1	1,0	0,5	0,5
Lighting of the biogas plant territory	1,0	1	1,0	8,0	8,0
Spot light for digesters inspection windows	0,1	1	0,1	0,5	0,0
Working lighting of switchboard	0,1	1	0,1	0,5	0,1
Total installed power, kW			228		
Total consumed electric energy, kWh per day					3488
Total consumed power, kW					145

Biogas upgrading plant							
Name equipment	Instal. Pow. (kW)	Q-y (pcs)	Total installed power (kW)	Working hours per day	Consumption kWh per day		
Biogas upgrading plant	170	1	170	24,0	4080		
Biomethane compressor plant	140	1	140	24,0	3360		
Total installed power, kW		•	310		•		
Total consumed electric energy, kWh per day				•	7440		
Average consumed electric power, kW					310		
Total average consumed electric power, kW					455		



Appendix 5

Prices for Zorg' services and equipment (part I)

#### Discounted Discounted Number of Discounts Name Pos price sub-total, price, unit price, FIIR FIIR Α Project documention 1 69000 0% 69000 69000 Supervision 1 35000 0% 35000 35000 С Startup and training 35000 0% 35000 35000 1 D Living and travel expences 40000 0% 40000 40000 1 Delivery of the equipment 10000 10000 40000 Ε 4 0% 1 Solid feeder (dosing buffer machine) 145000 0% 145000 145000 1 2 Screw conveyor 1 144000 0% 144000 144000 3 Digester vertical mixer 5 78000 390000 78000 0% Frame for Digester vertical mixer pos 3 5 6000 0% 6000 30000 4 5 Substrate pump 27000 27000 27000 1 0% Biogas blower 1 100 m3/h 2 22700 0% 22700 45400 7 Automation and electric cabinet 1 0% 145000 145000 145000

#### Appendix 6

#### Prices for equipment (part II )

	11 7					
Pos	Name		Unit price,	Discounts		Discounted price
		of units	EUR	*	price, EUR	sub-total, EUR
8	Gasholder	1	78000	0%	78000	78000
9	Over- and under pressure safeguard	1	5100	0%	5100	5100
10	Sight glasses/viewing windows with projector	1	4900	0%	4900	4900
11	Digested substrate pump	1	21000	0%	21000	21000
12	Filtrate supply pump	1	21000	0%	21000	21000
13	Substrate separation unit	1	44000	0%	44000	44000
14	Submersible mixer for receiving tank	1	11000	0%	11000	11000
15	Submersible mixer with guiding unit for filtrate tank	1	8000	0%	8000	8000
16	Biogas chiller (Biogas cooling system)	1	104000	0%	104000	104000
17	Desulphurization column with active coal 300 kg	1	35000	0%	35000	35000
18	Gas conditioning unit	1	16000	0%	16000	16000
19	Biogas burner	1	85000	0%	85000	85000
20	Heat supply station	1	37000	0%	37000	37000
21	Sensors (set)	1	50000	0%	50000	50000
22	Water supply and canalization system	1	27000	0%	27000	27000
23	Gas analyzer	1	27000	0%	27000	27000
24	Dry-cooler (Substrate cooling system for fermenter)	1	26000	0%	26000	26000

Total budget Zorg + Client

	Total Bauget Loig : Ottolic		i de le consenio						
#	Title	Cost	Value	Comments					
Α	Project documentation	69000	Euro	ZORG					
В	Supervision and adjustment	35000	Euro	ZORG					
С	Start-up and training	35000	Euro	ZORG					
D	Living and travel expenses	40000	Euro	ZORG					
E	Delivery (4 containers x 10000 EUR)	40000	Euro	ZORG					
Pos 01-07	Equipment part I	926400	Euro	ZORG					
Pos 08-24	Equipment part II	600000	Euro	ZORG					
25	Biomethane upgrading plant	600000	Euro	local					
26	Biomethane compressor plant	200000	Euro	local					
F	Laboratory	25000	Euro	local					
G	Construction	800000	Euro	local					
Н	Napier grass bagger machinary	125000	Euro	local					
I	Filtrate Storage (V=2000 m3)	20000	Euro	local					
J	Weight control (truck scale)	35000	Euro	local					
	Total without subsidy	3550400	Euro						
	Subsidy	-800000	Euro						
	Total with subsidy	2750400	Euro						
	Zorg' part (pos. A-E, 1-24)	1745400	Euro	49%					
	Client' part if no subsidy (pos. 25-26, F-J)	1805000	Euro	51%					

Initial Data	
Daily of raw materials, t	122
Amount of raw materials, t	44.641
Cost of raw materials, euro/t	
Total cost of raw materials per year, euro	698.325
Biogas output from 1 t of raw material, m3 Total annual biogas output, m3	9.733.332
Biomethane equivalent 1m3	9.733.332
biometiane equivalent ims	0,55
Biomethane module working days per year Elec. energy for own needs per year, kWh	360 3.931.200
Total annual biomethane production, t/per year	3.700

ეა				
60	Biogas, m3/day	Biomethane, m3/day	Biomethane, t/day	El.pow self consum, kV
00	26.667	14.220	10,3	455,0
00				

s, m3/day	Biomethane, m3/day	Biomethane, t/day	El.pow self consum, kW	Biofertlizer, t
6.667	14.220	10,3	455,0	20,0

Trace elements

0,0030

1,1 20.000,00 21.600

Activated carbon

0,08 1.800,00 135

.....

Economic effect	
IRR	105%
NPV, euro	3.097.819
Payback period, years	1,9
Discounted payback period, years	2,0
Cummulative net profit, euro	6.256.474
Cost of 1 t of biomethane, Euro	312,56
Cost of production of 1000 m3 of biogas, Euro	117,20

Cost of 1t biofertlizer, euro	0.00
Cost of 1 t of biomethane. euro	730.00
Cost of 1 kWh (el.power), euro	0,1000
Cost of biogas plant with VAT, euro	2.750.400
Net profit tax	20,0%
Value Added Tax	18,0%
Value Added Tax WACC	18,0% 10,92%

Equity investment	Bank financing	
20%	80%	
550.080	2.200.320	Sum
13,0%	13,0%	Interest rate

iron hydroxide

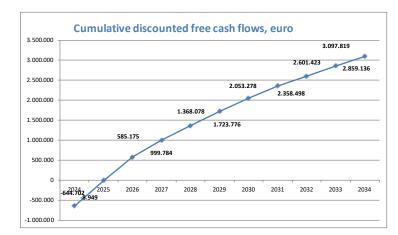
0,3 108,0 80,0 8.640

Napier grass

122,0 44.530 15,0 667.950

218,6 9.733.332

Incoming balance         0         3.550.400         3.195.360         2.875.824         2.588.242         2.329.417         2.096.476         1.886.828         1.698.145           Amortization         10%         0         355.040         3195.360         287.582         258.242         232.942         209.648         188.683         169.815           Outcoming balance         3.550.400         3.195.360         2.875.824         2.588.242         2.329.417         2.096.476         1.886.828         1.698.145         1.528.331	
Outcoming balance         3.550.400         3.195.360         2.875.824         2.588.242         2.329.417         2.096.476         1.886.828         1.698.145         1.528.331	1.528.331 1.375.49
×	152.833 137.55
	1.375.498 1.237.94
Cash-Flows 2024 2025 2026 2027 2028 2029 2030 2031 2032	2033 203
Gross revenue from biomethane + biofertlizer 0 2.700.652 2.700.652 2.700.652 2.700.652 2.700.652 2.700.652 2.700.652 2.700.652 2.700.652	2.700.652 2.700.65
Net revenue from biomethane production 0 2.700.652 2.700.652 2.700.652 2.700.652 2.700.652 2.700.652 2.700.652 2.700.652 2.700.652	2.700.652 2.700.65
Operating costs 0 -1.139.541 -1.139.541 -1.139.541 -1.139.541 -1.139.541 -1.139.541 -1.139.541 -1.269.285	-1.139.541 -1.139.54
Raw materials cost 0 -698.325 -698.325 -698.325 -698.325 -698.325 -698.325 -698.325 -698.325	-698.325 -698.32
Biogas plant service 0 -13.896 -13.896 -37.056 -13.896 -13.896 -21.896 -13.896 -13.896 -13.896 -13.896 -13.896	-13.896 -13.89
Biomethane module service 0 -9.000 -9.000 -9.000 -24.000 -9.000 -9.000 -9.000 -0.000 -0.000	-9.000 -9.00
Elec, energy for own needs 0 -393.120 -393.120 -393.120 -393.120 -393.120 -393.120 -393.120 -393.120 -393.120	-393.120 -393.12
Salaries 0 -25.200 -25.200 -25.200 -25.200 -25.200 -25.200 -25.200 -25.200 -25.200	-25.200 -25.20
wear out of equipment, % 1,5 1,5 1,5 1,5 1,5 1,5 1,5 1,5 1,5 1,5	1,5
EBITDA 0 1.561.111 1.561.111 1.561.111 1.522.951 1.561.111 1.561.111 1.561.111 1.431.367	1.561.111 1.561.11
EBITDA margin 58% 58% 58% 58% 58% 58% 58% 58% 58% 58%	58% 58
Finance expenses -165.024 -271.740 -243.135 -214.531 -185.927 -157.323 -128.719 -100.115 -85.812	-57.208 -28.60
VAT -287.156 -287.156 -287.156 -287.156 -287.156 -287.156 -287.156 -272.982	-287.156 -287.15
VAT credit balance -800.000 -287.156 -287.156 -287.156 -287.156 -287.156 -287.156 -272.982	-287.156 -287.15
Profit before tax -165.024 1.289.371 1.317.975 1.346.579 1.337.023 1.403.788 1.432.392 1.460.996 1.345.554	1.503.902 1.532.50
Net profit tax 0 0 0 -211.799 -215.640 -234.169 -244.549 -254.463 -235.148	-270.214 -278.99
Net profit -165.024 1.002.215 1.030.819 847.624 838.397 882.463 900.687 919.377 837.424	946.532 966.35
Net margin 37% 38% 31% 31% 33% 33% 34% 31%	35% 36
Own investment -550.080	
Loan repayment 0 -220.032 -220.032 -220.032 -220.032 -220.032 -220.032 -220.032 -220.032 -220.032 -220.032	-220.032 -220.03
Free Cash Flows -715.104 782.183 810.787 627.592 618.365 662.431 680.655 699.345 617.392	726.500 746.32
Cumulative free fash flows -715.104 67.079 877.866 1.505.458 2.123.823 2.786.253 3.466.908 4.166.254 4.783.646	5.510.147 6.256.47
Period (years) 1 2 3 4 5 6 7 8 9	10 0.250.47
• /	
	35% 329
Discount Factor 90% 81% 73% 66% 60% 54% 48% 44% 39%	
Discount Factor         90%         81%         73%         66%         60%         54%         48%         44%         39%           Discounted Free Cash Flows         644.702         635.753         594.124         414.608         368.295         355.698         329.502         305.220         242.925	257.714 238.68
	<b>257.714 238.68 2.859.136 3.097.81</b>
Discounted Free Cash Flows         -644.702         635.753         594.124         414.608         368.295         355.698         329.502         305.220         242.925           Cumulative discounted free cash flows         -644.702         -8.949         585.175         999.784         1.368.078         1.723.776         2.053.278         2.358.498         2.601.423	2.859.136 3.097.81
Discounted Free Cash Flows         -644.702         635.753         594.124         414.608         368.295         355.698         329.502         305.220         242.925           Cumulative discounted free cash flows         -644.702         -8.949         585.175         999.784         1.368.078         1.723.776         2.053.278         2.358.498         2.601.423           Bank credit amortization         2024         2025         2026         2027         2028         2029         2030         2031         2032	2.859.136 3.097.81 2033 203
Discounted Free Cash Flows         644.702         635.753         594.124         414.608         368.295         355.698         329.502         305.220         242.925           Cumulative discounted free cash flows         -644.702         -8.949         585.175         999.784         1.368.078         1.723.776         2.053.278         2.358.498         2.601.423           Bank credit amortization         2024         2025         2026         2027         2028         2029         2030         2031         2032           Starting debt dalance         0         2.200.320         1.980.288         1.760.256         1.540.224         1.320.192         1.100.160         880.128         660.096	2.859.136 3.097.81
Discounted Free Cash Flows         644.702         635.753         594.124         414.608         368.295         355.698         329.502         305.220         242.925           Cumulative discounted free cash flows         -644.702         -8.949         585.175         999.784         1.368.078         1.723.776         2.053.278         2.358.498         2.601.423           Bank credit amortization         2024         2025         2026         2027         2028         2029         2030         2031         2032           Starting debt dalance         0         2.200.320         1.980.288         1.760.256         1.540.224         1.320.192         1.100.160         880.128         660.096           Credit drawdowns         2.200.320         2.200.3	2.859.136     3.097.81       2033     202       440.064     220.03
Discounted Free Cash Flows         644.702         635.753         594.124         414.608         368.295         355.698         329.502         305.220         242.925           Cumulative discounted free cash flows         -644.702         -8.949         585.175         999.784         1.368.078         1.723.776         2.053.278         2.358.498         2.601.423           Bank credit amortization         2024         2025         2026         2027         2028         2029         2030         2031         2032           Starting debt dalance         0         2.200.320         1.980.288         1.760.256         1.540.224         1.320.192         1.100.160         880.128         660.096	2.859.136 3.097.81 2033 203
Discounted Free Cash Flows         644.702         635.753         594.124         414.608         368.295         355.698         329.502         305.220         242.925           Cumulative discounted free cash flows         -644.702         -8.949         585.175         999.784         1.368.078         1.723.776         2.053.278         2.358.498         2.601.423           Bank credit amortization         2024         2025         2026         2027         2028         2029         2030         2031         2032           Starting debt dalance         0         2.200.320         1.980.288         1.760.256         1.540.224         1.320.192         1.100.160         880.128         660.096           Credit drawdowns         2.200.320         220.032         220.032         220.032         220.032         220.032         220.032         220.032         220.032         220.032         220.032         220.032         220.032         220.032         220.032         220.032         220.032         220.032         20.032         20.032         20.032         20.032         20.032         20.032         20.032         20.032         20.032         20.032         20.032         20.032         20.032         20.032         20.032         20.032         20.032 </td <td>2.859.136 3.097.81  2033 203  440.064 220.03  220.032 220.032</td>	2.859.136 3.097.81  2033 203  440.064 220.03  220.032 220.032
Discounted Free Cash Flows         644.702         635.753         594.124         414.608         368.295         355.698         329.502         305.220         242.925           Cumulative discounted free cash flows         -644.702         -8.949         585.175         999.784         1.368.078         1.723.776         2.053.278         2.358.498         2.601.423           Bank credit amortization         2024         2025         2026         2027         2028         2029         2030         2031         2032           Starting debt dalance         0         2.200.320         1.980.288         1.760.256         1.540.224         1.320.192         1.100.160         880.128         660.096           Credit drawdowns         2.200.320         220.032	2.859.136 3.097.81  2033 203  440.064 220.03  220.032 220.032



# Implementation terms and payment

Months	_	2	က	7	വ	9	7	8	6	10	11	12
Project documentation	20%	%09										
Approvals and permits												
Equipment supply	20%		20%		20%		10%					
Biogas upgrading plant												
Construction												
Supervision	20%					20%						
Biogas plant start-up										%09	25%	25%

## Contracts

Project implementation is executed simultaneously under several contracts

- Engineering contractEquipment supply contract
  - Supervision contract
- Start-up and training contract

#### List of exclusions

#### for a 10 tpd bioCNG plant:

- 1) Import taxes and local duties in India. The importer needs to apply the Ministry of Economy of India. To get waiving of the import duties. Biogas plant is a plant for renewables.
- 2) Project report, civil permits and authorizations, adaptation of the project documentation by a licensed local engineering organisation for the permit purposes. Namely the organisation puts their stamp and acts act the face of the project. The design documentation is not changed in fact. 10 000 15 000 EUR
- 3) Topographic and geological surveys 3000-7000 EUR
- 4) Electric transformer and the external electric line 150 kW for start-up, for construction period and 450 kW for normal operation.
- 5) Construction and installation materials and works, namely 0,8 million EUR, mentioned on the pages 39-40 of the proposal. Zorg provides prelim drawings and bill of quantities for your evaluation and our fore cast verification.
- 6) External roads,
- 7) Temporary water supply during the construction and the hydraulic test of reactors at least 500 m3 water per day. It can be a technical quality water from a river, lake, well. Not salty.
- 8) Bacterial seed for the start-up. It can be biomass from another biogas plant. Possibley also cow manure, any kind of manure, sludge from city sewage treatment plant. Customer needs to bring the seed one-time during a 1-2 week period and to fill with it at least 15-20% of the reactor volume 600-800 m3. The rest is filled with the water item 7 above.
- 9) Machinery to transport Napier grass to and from silage storage to the solid feeders (a truck, a frontal loader, a tractor)
- 10) Machinery to transport filtrate and the digested mass from the biogas plant to the agricultural fields (a truck, a frontal loader, a tractor)
- 11) Pos. 25-26 page 39: biogas to bioCNG purification (namely CO2 removal), gas cylinder cascades 200-250 bars, a truck for gas cylinders, gas fuelling station, bioCNG gas storage, a chromatograph,
- 12) oxygen generator 20 liter pro min for the desuphur system in order to keep the definite O2 and N level in the end-gas. If the requirements are not strict air can be used.
- 13) Oxidation of the refuse CO2 gas.
- 14) Liquefaction and storages of CO2
- 15) Activated carbon 0.3 tonne per year x 1800 EUR/tonne
- 16) Fe(OH)3, Fe(OH)2 110 tonnes per year x 80 EUR/tonne = 8 800 EUR
- 17) Anti-foam reagent 2 tonnes annually (all kinds of vegetable oil, for example, palm oil or rapeseed oil)
- 18) PE foil for the silage storage in bags
- 19) Demineralized water to the heating system 1,5 tonnes,
- 20) Spare parts 70 000 EUR for 2 years



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